(FILE 'HOME' ENTERED AT 14:39:24 ON 24 MAY 2006)

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      FILE WPIFV
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FILE 'BIOSIS, EMBASE, MEDLINE, SCISEARCH, CAPLUS, BIOTECHNO, PASCAL, DGENE, PROMT, ESBIOBASE, IFIPAT, TOXCENTER' ENTERED AT 14:40:39 ON 24 MAY 2006

61

FILE WPINDEX
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T.1

L3	419 S L2 AND RECOMBINANT
L4	93 S L3 AND PURIF?
L5	19 S L4 AND 99%
L6	16 DUP REM L5 (3 DUPLICATES REMOVED)
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=> d 16 ibib ab 1-16

ANSWER 1 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN

11091341 IFIPAT; IFIUDB; IFICDB AN

TITLE: METHODS FOR PRODUCING AND PURIFYING

RECOMBINANT ALPHA-L-IDURONIDASE

INVENTOR(S): Chan; Wai-Pan, Castro Valley, CA, US

Chen; Lin, San Francisco, CA, US Fitzpatrick; Paul A., Albany, CA, US Henstrand; John M., Davis, CA, US Kakkis; Emil D., Novato, CA, US Qin; Minmin, Pleasanton, CA, US Starr; Christopher M., Sonoma, CA, US Wendt; Dan J., Walnut Creek, CA, US Zecherle; Gary N., Novato, CA, US

PATENT ASSIGNEE(S):

Unassigned

AGENT:

MARSHALL, GERSTEIN & BORUN LLP, 233 S. WACKER DRIVE,

SUITE 6300, SEARS TOWER, CHICAGO, IL, 60606, US

NUMBER PK DATE -----\_\_\_\_\_ US 2006040348 A1 · 20060223 PATENT INFORMATION: APPLICATION INFORMATION: US 2003-722371 20031124

GRANTED PATENT NO.

OR STATUS APPLN. NUMBER DATE

---------------US 2001-993038 20011113 ABANDONED

CONTINUATION OF: FAMILY INFORMATION:

US 2006040348 20060223

DOCUMENT TYPE:

Utility

Patent Application - First Publication

FILE SEGMENT:

CHEMICAL

APPLICATION

PARENT CASE DATA:

This application claims priority to U.S. application Ser. No. 09/711,202, filed Nov. 9, 2000, which is a continuation-in-part of U.S. patent application Ser. No. 09/439,923, filed Nov. 12, 1999.

NUMBER OF CLAIMS:

28

AB The present invention provides a recombinant human alpha -Liduronidase and biologically active fragments and muteins thereof with a purity greater than 99%. The present invention further provides large-scale methods to produce and purify commercial grade recombinant human alpha -L-iduronidase enzyme thereof.

L6 ANSWER 2 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN 04404900 IFIPAT; IFIUDB; IFICDB ΑN

TITLE: RECOMBINANT ALPHA-L-IDURONIDASE,

METHODS FOR PRODUCING AND PURIFYING THE

SAME AND METHODS FOR TREATING DISEASES CAUSED BY

DEFICIENCIES THEREOF

Kakkis; Emil D., 2572 Laguna Vista Dr., Novato, CA, INVENTOR(S):

94949, US

Tanamachi; Becky, 3343 Walnut Ave., Signal Hill, CA,

90809, US

PATENT ASSIGNEE(S):

Unassigned Rao, Manjunath N

PRIMARY EXAMINER:

Marshall, Gerstein & Borun LLP

AGENT:

NUMBER PK DATE

PATENT INFORMATION: US 7041487 B2 20060509 US 2003013179 A1 20030116

US 2003013179 A1 20030116 APPLICATION INFORMATION: US 2002-206443 20020725

EXPIRATION DATE: 12 Nov 2019

GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

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CONTINUATION OF: US 1999-439923 19991112 6426208

FAMILY INFORMATION: US 7041487 20060509

US 6426208

DOCUMENT TYPE: Utility

Granted Patent - Utility, with Pre-Grant Publication

FILE SEGMENT: CHEMICAL

GRANTED

#### PARENT CASE DATA:

This application is a continuation application of U.S. patent application Ser. No. 09/439,923, filed Nov. 12, 1999, now U.S. Pat. No. 6,426,208, issued Jul. 30, 2002, which is incorporated herein by reference.

NOTE: Subject to any Disclaimer, the term of this patent is

extended or adjusted under 35 USC 154(b) by 326 days.

This Patent is subject to a Terminal Disclaimer.

NUMBER OF CLAIMS: 33

GRAPHICS INFORMATION: 11 Drawing Sheet(s), 15 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA

encoding alpha-L-iduronidase (SEQ ID Nos: 1 and 2). Nucleotides 1

through 6200 are provided. Amino acids are provided starting with the first methionine in the open reading frame.

FIG. 2 represents the results from an SDS-PAGE run of eluate obtained according to the procedure set forth in Example 1. Lane 1 is blank. Lane 2 contained high molecular weight standards. Lane 3 is a blank. Lane 4 contained bovine serum albumin in a concentration of 50 mu g. Lanes 5 through 10 represent eluate containing recombinantly produced human alphaL-iduronidase

in amounts of 1 mu g, 2 mu g, 5 mu g, 5 mu g, 5 mu g and 5 mu g, respectively. FIG. 3 reveals the urinary GAG levels in 16 MPS I patients in relation to normal excretion values. There is a wide range of urine GAG values in untreated MPS I patients. A greater than 50% reduction in excretion of undegraded GAGs following therapy with recombinant alpha-L-iduronidase is a

valid means to measure an individual's response to therapy.

FIG. 4 demonstrates leukocyte iduronidase activity before and after enzyme therapy in MPS I patients.

FIG. 5 demonstrates the buccal iduronidase activity before and after enzyme therapy.

FIG. 6 demonstrates in three patients that a substantial shrinkage of liver and spleen together with significant clinical improvement in joint and soft tissue storage was associated with a greater than 65% reduction in undegraded GAG after only 8 weeks of treatment with **recombinant** enzyme.

FIG. 7 demonstrates that there is substantial normalization of livers (FIG. 7A) and spleens (FIG. 7B) in patients treated with **recombinant** enzyme after only 12 weeks of therapy.

FIG. 8 demonstrates a precipitous drop in urinary GAG excretion over 22 weeks of therapy with **recombinant** enzyme in 6 patients.

The present invention provides a recombinant alpha
-Liduronidase and biologically active fragments and mutants thereof,
methods to produce and purify this enzyme as well as methods to
treat certain genetic disorders including- alpha -Liduronidase deficiency
and mucopolysaccharidosis I (MPS 1).

ANSWER 3 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN L6

10982027 IFIPAT; IFIUDB; IFICDB AN

VIRAL VECTORS AND METHODS FOR PRODUCING AND USING THE TITLE:

SAME

INVENTOR (S): Amalfitano; Andrea, Durham, NC, US

Koeberl; Dwight D., Durham, NC, US Sun; Baodong, Morrisville, NC, US

PATENT ASSIGNEE(S): Unassigned

JENKINS, WILSON & TAYLOR, P. A., 3100 TOWER BLVD, AGENT:

SUITE 1400, DURHAM, NC, 27707, US

NUMBER PK DATE \_\_\_\_\_ PATENT INFORMATION: US 2005220766 A1 20051006 APPLICATION INFORMATION: US 2003-511980 20030430 WO 2003-US13323 20030430

20050407 PCT 371 date 20050407 PCT 102(e) date

DATE NUMBER -----

US 2002-376397P 20020430 (Provisional)
US 2005220766 20051006 PRIORITY APPLN. INFO.:

FAMILY INFORMATION:

DOCUMENT TYPE: Utility

Patent Application - First Publication

FILE SEGMENT: CHEMICAL

APPLICATION

## GOVERNMENT INTEREST:

This work was supported by grant R01-DK 52925 from the U.S. National Institute of Health. Thus, the U.S. government has certain rights in the invention.

# PARENT CASE DATA:

This application is based on and claims priority to U.S. Provisional Application Ser. No. 60/376,397, filed Apr. 30, 2002, herein incorporated by reference in its entirety.

NUMBER OF CLAIMS:

142 17 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1A is a schematic of a hybrid Ad-AAV vector containing the chicken beta-actin (CB) promoter driving the hGAA cDNA. The hybrid vector, AdAAVCBGAApA, was constructed by bacterial recombination. The packaging size for the AAV vector sequence is 4.4 kb.

FIG. 1B is an autoradiograph depicting Southern blot analysis of DNase I-resistant hybrid Ad-AAV vector particles (Ad-AAV hybrid) , the plasmid containing the AAV vector sequences prior to bacterial recombination to produce Ad particles (pShuttle-AAV), and the AAV vector plasmid (pAAVCBGAApA). DNA was analyzed with AhdI and BssHII to determine that the AAV TR sequences were present (not deleted during recombination). AhdI cuts once in each terminal repeat and BssHII cuts twice in each terminal repeat, and each restriction digest gives unique fragments that were present in the recombinant Ad-AAV DNA.

FIG. 1C is a photograph of a cesium chloride gradient of hybrid Ad-AAV vector particles. Two viral bands were present, which eqilibrated at positions below a layer of protein at the top of the gradient.

FIG. 1D is an autoradiograph depicting Southern blot analysis of the two viral bands in FIG. 1C. Vector DNA was treated with DNase I and extracted prior to restriction enzyme analyis and Southern blotting. Each sample was 10 mu 1. Lanes (11)-(16) contain linearized Ad5-containing plasmid representing the indicated number of double-stranded (ds) Ad particles. Therefore, the vector stock purified from the lower band contained 3.1x1011 DNase

```
I-resistant Ad-AAV vector particles per ml (lanes 6-9).
FIG. 1E is a schematic of a hybrid Ad-AAV vector packaging method for AAV
vector purification. 293 cells were transfected with split AAV helper
plasmids and transduced with a hybrid AdAAV vector containing the AAV vector
sequences. No contaminating modified Ad vector is replicated by 293 cells
(Amalfitano et al. (1998) J. Virol. 72:926-933). The AAV vector was
                by heparin-agarose column method (Zolotukhin et al. (1999)
***purified***
Gene Ther. 6:973-985).
FIG. 2A is an autoradiograph of a Southern blot depicting AAV vector packaging
with an Ad-AAV hybrid vector. For the transfection-only method, 293 cells were
transfected with plasmids containing the AAV rep and cap genes driven by
heterologous promoters (Allen et al. (2000) Mol. Ther. 1:88-95) and with the
AAV vector plasmid and pLNCorf6 (Scaria et al. (1995) Gene Ther. 2:295-298)
(lane 1 only). For the hybrid AdAAV method of AAV vector packaging, the cells
were transduced with the indicated number of hybrid Ad-AAV vector DNase-I
resistant particles, and transfected with plasmids containing the AAV rep and
cap genes (as shown in FIG. 1D). The Southern blot shows the yield of DNase
I-resistant single-stranded AAV vector genomes per cell for each condition.
Each sample represented 6x105 293 cells. Lanes (7) to (11) contained vector
plasmid, digested with BqIII to release the double-stranded AAV vector
sequences, representing the indicated number of singlestranded (ss) AAV vector
particles.
FIG. 2B is a bar graph showing that AAV-CBGAAPA was packaged with different Ad
and AAV helpers. Five conditions for packaging of AAV-CBGAAPA were evaluated,
including transfection of pAAV-CBGAApA plus split AAV helper plasmids and
pLNCorf6 (adapted from Allen et al., 2000), hybrid Ad-AAV transduction plus
transfection of split AAV helper plasmids, modified Ad ((E1-,polymerase-
)AdCMVLacZ) transduction plus split transfection of split AAV helper plasmids,
wild-type Ad5 infection plus tranfection of pACG2 (Xiao et al. (1998) J. Virol.
72:10222-10226) and pAAV-CBGAApA, and hybrid Ad-AAV transduction plus
transfection of pACG2.
FIG. 2C is an autoradiograph of a Southern blot that was performed to quantify
the contaminating Ad-AAV genomes. Lanes as follows: (1) untreated 293 cells,
(2) transfection of pMVCBGAApA plus split AAV helper plasmids and pLNCorf6
(adapted from Allen et al. 2000), (3) hybrid Ad-AAV transduction plus
transfection of split AAV helper plasmids, (4) modified Ad ((E1, polymerase-
)AdCMVLacZ) transduction plus split transfection of split AAV helper plasmids,
(5) wild-type Ad5 infection plus tranfection of pACG2 (Xiao et al. (1998) J.
Virol. 72:1022210226) and pAAV-CBGAApA, and (6) hybrid Ad-AAV transduction plus
transfection of pACG2, (7) no sample, and (8)-(12) linearized Ad5-containing
plasmid representing the indicated number of double-stranded (ds) Ad particles.
Each sample represented 6x105 293 cells.
FIG. 3A is a bar graph depicting analysis of large-scale AAV vector packaging
with an Ad-AAV hybrid vector. The yield of DNase I-resistant AAV vector
particles for AAV-CBGAApA packaged by transfection of pLNCorf6, or transduction
with the Ad-AAV hybrid to provide Ad helper functions, compared to a vector
encoding glucose-6-phosphatase, AAV-CBcG6PpA, packaged with pLNCorf6. Twenty to
40 plate vector preparations were purified (3 vector preparations per
condition), and the yield was calculated per cell plated. The mean number of
AAV vector particles per cell is shown with the standard deviation indicated.
FIG. 3B is an autoradiograph of a Southern blot analysis of AAVCBGAApA
***purification*** , quantified versus titrated vector plasmid DNA. The
samples represent vector DNA extracted from 25 microliters of sample. Standard
amounts of vector plasmids were loaded for quantitation of vector particles.
Lanes represent the following samples: (1) Crude cell lysate, (2) 40% iodoxinal
fraction (3) Heparin-agarose (HA) column flow-through, (4) HA column wash, (5)
HA column eluate fraction (ef) 1, (6) HA column ef 2, (7) HA column ef 3, (8)
HA column ef 4, (9) HA column ef 2 after dialysis (10) HA column ef 2 plus
2.5x1010 particles AAV vector plasmid, (11) HA column ef 2 plus 2.5x1010
particles AAV vector plasmid, no DNase I added, (12)-(18) vector plasmid
```

representing the indicated number of singlestranded (ss) AAV vector particles.

Therefore, the purified AAV vector stock contained 4.8x1011 DNase

I-resistant vector particles per ml.

FIG. 3C is an autoradiograph of a Southern blot analysis that quantitated the contaminating Ad-AAV genomes in the samples described in FIG. 3B above. Lanes 10-18 differed as follows: (10) HA column ef 2 plus 2.5x109 particles Ad-containing plasmid, (11) HA column ef 2 plus 2.5x109 particles Adcontaining plasmid, no DNase I added, (12) No sample, (13)-(17) linearized Ad5-containing plasmid representing the indicated number of double-stranded (ds) Ad particles. The residual AdAAV in the AAV vector stock was reduced to less than 1 infectious particle per 1010 AAV vector particles. FIG. 4A depicts Western blot analysis of plasma that was performed at 3 days following intravenous administration of the hybrid Ad-AAV (essentially Ad) vector encoding hGAA (2x1010 vector particles/mouse). Recombinant hGAA (rhGAA) is shown for reference (2 ng total), and the 110 kD hGAA precursor was detected as expected (Amalfitano et al. (1999) Proc. Natl. Acad. Sci. U.S.A. 96:8861-8866, Ding et al. (2001) Hum. Gene Ther. 12:955-965). FIG. 4B depicts Western blot analysis of GAA-KO mice that received a hybrid Ad-AAV vector (2x1010 DNase I-resistant vector particles) or an AAV vector (4x1010 DNase I-resistant vector particles or 1x1012 DNase I-resistant vector particles) encoding hGAA by intravenous administration. Western blot analysis of liver is shown at 2 and 6 weeks after vector administration for each group (n=3 for each group). (Note: hGAA in mouse liver migrates slightly faster than rhGAA.) GAA-KO mice that received an AAV vector (1x1012 vector particles) encoding hGAA by intravenous administration (n=2) shown 6 weeks after vector administration. Untreated, affected GAA-KO mouse liver is shown for comparison (No vector, n=2). For the higher number of AAV vector particles, the 67 kD, 76

FIGS. 5A-5C depict human GAA secretion and uptake following portal vein injection of an AAV vector in GAA-KO mice.

FIG. 5A depicts Western blot analysis of plasma from GAAKO SCID mice at the indicated times following portal vein injection of the indicatedAAV vector encoding hGAA, and from untreated, GAAKO SCID mice (Controls). Each lane represents an individual mouse.

FIG. 5B is a bar graph that summarizes GAA analysis for tissues following portal vein injection of an AAV vector. GAA-KO/SCID mice received the vector packaged as AAV2 (n=1) or AAV6 (n=1). Controls were age-matched, untreated GAA-KO/SCID mice (n=2). The GM level was analyzed twice, independently, and the average and range are shown.

kD, and 110 kD hGAA species were detected as expected (Amalfitano et al. (1999) Proc. Nat. Acad. Sci. U.S.A. 96:8861-8866, Ding et al. (2001) Hum. Gene Ther.

FIG. 5C is a photomicrograph depicting periodic acid Schiff (PAS) staining of the heart for a GAA-KO/SCID mouse that received an AAV vector (left panel AAV-CBGAAPA) and for an untreated GAA-KO/SCID mouse (right panel) and HE staining (lower panels). Magnification 100x.

A recombinant hybrid virus, including: (a) a deleted adenovirus vector genome comprising the adenovirus 5' and 3' cis-elements for viral replication and encapsidation, and further comprising a deletion in an adenovirus genomic region selected from the group consisting of: (i) the polymerase region, wherein said deletion essentially prevents the expression of a functional polymerase protein from said deleted region and said hybrid virus does not otherwise express a functional polymerase protein, (ii) the preterminal protein region, wherein said deletion essentially prevents the expression of a functional preterminal protein from said deleted region, and said hybrid virus does not otherwise express a functional preterminal protein, and (iii) both the regions of (i) and (ii); and (b) a recombinant adeno-associated virus (AAV) vector genome flanked by the adenovirus vector genome sequences of (a), said recombinant AAV vector genome comprising (i) AAV 5' and 3' inverted terminal repeats, (ii) an AAV packaging sequence, and (iii) a heterologous nucleic acid sequence, wherein said heterologous nucleic acid sequence is flanked by the 5' and the 3' AAV inverted terminal repeats of (i). Methods of making and using the recombinant hybrid virus are also disclosed.

12:955-965).

10919552 IFIPAT; IFIUDB; IFICDB AΝ

METHODS AND COMPOSITIONS FOR THE PRODUCTION OF TITLE:

ADENOVIRAL VECTORS

Pham; Hai, Houston, TX, US INVENTOR(S):

Zhang; Shuyuan, Sugar Land, TX, US

PATENT ASSIGNEE(S): Unassigned

FULBRIGHT & JAWORSKI L.L.P., 600 CONGRESS AVE., SUITE AGENT:

2400, AUSTIN, TX, 78701, US

NUMBER PK DATE PATENT INFORMATION: US 2005158283 A1 20050721 APPLICATION INFORMATION: US 2005-79986 20050315

GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

DIVISION OF: US 2003-439278 20030515 PENDING FAMILY INFORMATION: US 2005158283 20050721 DOCUMENT TYPE:

Patent Application - First Publication

FILE SEGMENT: CHEMICAL APPLICATION

NUMBER OF CLAIMS: 62 7 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1A show results of a study demonstrating the effect of temperature on Adp53 production (vp/flask).

FIG. 1B shows results of a study demonstrating the effect of temperature on Admda7 production (vp/flask).

FIG. 2. Cell growth and viability in the bioreactor.

FIG. 3. Glucose and lactate concentrations (q/L) in media vs. days in culture.

FIG. 4. Diagram of a perfusion bioreactor system.

FIG. 5. Cell growth and viability in perfusion culture vs. days in culture.

FIG. 6. Glucose and lactate concentrations (g/L) in perfusion culture vs. days in culture.

The present invention addresses the need to improve the yield of AB adenovirus when grown in cell culture systems. In particular, it has been demonstrated that for adenovirus, the use of infection temperatures lower than 37 degrees C. in a cell culture system results in improved yields of adenovirus. In addition, it has been demonstrated that when host cells are grow in a bioreactor, initiating adenovirus infection by diluting the host cells with fresh media and adenovirus results in improved yield of adenovirus. Methods of adenoviral production and purification using infection temperatures less than 37 degrees C. are disclosed. Methods of adenoviral production and purification wherein the host cells are grown in a bioreactor and adenovirus infection is initiated by diluting the host cells with fresh media and adenovirus are also disclosed.

T.6 ANSWER 5 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN AN 04202137 IFIPAT; IFIUDB; IFICDB

TITLE: METHODS FOR TREATING DISEASES CAUSED BY DEFICIENCIES

OF RECOMBINANT ALPHA-L-IDURONIDASE

INVENTOR(S): Kakkis; Emil D., 2512 Laguna Vista Dr., Novato, CA,

94949, US

PATENT ASSIGNEE(S): Unassigned PRIMARY EXAMINER: Rao, Manjunath N

AGENT: Marshall, Gerstein & Borun LLP

NUMBER PK DATE -----PATENT INFORMATION: US 6858206 B2 20050222 US 2002164758 A1 20021107 APPLICATION INFORMATION: US 2001-993241 20011113

EXPIRATION DATE: 12 Nov 2019

GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

CONTINUATION-IN-PART OF: US 1999-439923 19991112 6426208 CONTINUATION-IN-PART OF: US 2000-711205 20001109 6585971

FAMILY INFORMATION: US 6858206 20050222

US 6426208 US 6585971

US 2002164758 20021107

DOCUMENT TYPE: Utility

Granted Patent - Utility, with Pre-Grant Publication

FILE SEGMENT: CHEMICAL

GRANTED

#### PARENT CASE DATA:

This application is a continuation-in-part to U.S. patent application Ser. No. 09/711,205, filed on Nov. 9, 2000 now U.S. Pat. No. 6,585,971, Jul. 1, 2003 which is a continuation-inpart of U.S. patent application Ser. No. 09/439,923, filed on Nov. 12, 1999.

NOTE: Subject to any Disclaimer, the term of this patent is

extended or adjusted under 35 USC 154(b) by 203 days. MICROFILM REEL NO: 014767 FRAME NO: 0890

 014770
 0226

 014772
 0436

 015398
 0139

 015577
 0341

 015580
 0887

 015584
 0474

NUMBER OF CLAIMS: 46

GRAPHICS INFORMATION: 14 Drawing Sheet(s), 20 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA encoding alpha-L-iduronidase (SEQ ID NOS:1 and 2). Nucleotides 1 through 6200 are provided. Amino acids are provided starting with the first

through 6200 are provided. Amino acids are provided starting with the first methionine in the open reading frame.

FIG. 2 represents the results from SDS-PAGE runs of eluate obtained according to the procedures as described below. The top panel shows the SDS-PAGE results of purified alpha-Liduronidase (3 micrograms) and contaminants from

the production/ purification scheme disclosed in Kakkis, et al., Protein Expr. Purif. 5: 225-232 (1994). In the bottom panel, SDS-PAGE

results of purified alpha-L-iduronidase with contaminants

from an unpublished prior production/purification process (U.S.

patent application Ser. Nos. 09/078,209 and 09/170,977) referred to as the Carson method in Lanes 2 (7.5 microgram alpha-Liduronidase) and Lane 3 (5.0

microgram alpha-L-iduronidase) are compared to that of the

production/purification process of the present invention referred to as the Galli Process (Lane 4 5 micrograms alpha-L-iduronidase). Lane

1 contains the molecular weight marker. FIG. 2 shows that the Galli production/

\*\*\*purification\*\*\* method of the present invention yields a highly

\*\*\*purified\*\*\* alpha-L-iduronidase product with fewer contaminants in comparison with prior production/purification schemes.

FIG. 3 demonstrates the alpha-iduronidase production level over a 30-day period, during which time cells are switched at day 5 from a serum containing medium to a serum-free medium. alphaIduronidase production was characterized by: (1) absence of a need for adaptation when cells are switched from serumcontaining to serum-free medium at 100200 (top and bottom panels) with an uninterrupted increase in productivity (top panel); (2) a high level of

production in excess of 4 mg per liter (1000 per mL) in a protein-free medium (bottom panel); and (3) a boost in alpha-iduronidase production with butyrate induction events (bottom panel).

- FIG. 4 demonstrates a decrease in liver volume during enzyme therapy in MPS I
- FIG. 5 demonstrates urinary GAG excretion during enzyme therapy.
- FIG. 6 demonstrates elbow and knee extension in HAC002 during enzyme therapy.
- FIG. 7 demonstrates shoulder flexion to 104 weeks in four patients with the most restriction during enzyme therapy.
- FIG. 8 demonstrates improvement in sleep apnea before and after six weeks of therapy.
- FIG. 9 demonstrates the improvement in apneas and hypopneas during sleep with enzyme therapy in each individual patient.
- FIG. 10 demonstrates the improvement in pulmonary function tests before and after 12 and 52 weeks of enzyme therapy in one patient.
- FIG. 11 demonstrates increased height growth velocity with enzyme therapy.
- FIG. 12 shows the degree of contamination by Chinese Hamster Ovary Protein (CHOP) and degree of purity of alpha-Liduronidase, produced by (1) the Carson method, an unpublished prior production/purification process (U.S.
- patent application Ser. Nos. 09/078,209 and 09/170,977 and (2) the Galli method, the production/purification process of the present invention.
- FIG. 12 shows that alpha-L-iduronidase produced and purified by the Galli method has a higher degree of purity and lower degree of CHOP contamination in comparison to that of the Carson method.
- FIG. 13 shows a comparison of alpha-L-iduronidase produced by the Galli method versus the Carson method. On the left side of the Figure, results from a Western Blot show that the Galli material (left side, column 2) comprise fewer contaminating protein bands (between 48 kDa and 17 kDa) in comparison with the Carson material (left side, column 3). On the right side of the Figure, results from an SDS-PAGE silver stain show the absence of a band at the 62 kDa in the Galli material (column 2) in comparison to the presence of such a band in the Carson material (column 3).
- The present invention provides a formulation comprising a pharmaceutical composition comprising a human recombinant alpha -Liduronidase or biologically active or muteins thereof with a purity of greater than 99%, or in combination with a pharmaceutically acceptable carrier. The present invention further provides methods to treat certain genetic disorders including alpha -Liduronidase deficiency and mucopolysaccharidosis I (MPS 1) by administering said formulation.

ANSWER 6 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN ΑN 10722085 IFIPAT; IFIUDB; IFICDB

TITLE: METHODS AND COMPOSITIONS FOR THE PRODUCTION OF

ADENOVIRAL VECTORS

INVENTOR (S): Pham; Hai, Houston, TX, US

Zhang; Shuyuan, Sugar Land, TX, US

PATENT ASSIGNEE(S): Introgen Therapeutics, Inc., US

AGENT: FULBRIGHT & JAWORSKI L.L.P., 600 CONGRESS AVE., SUITE

2400, AUSTIN, TX, 78701, US

NUMBER PK DATE -----PATENT INFORMATION: US 2004229335 A1 20041118 APPLICATION INFORMATION: US 2003-439278 20030515 FAMILY INFORMATION: US 2004229335
DOCUMENT TYPE: 20041118 DOCUMENT TYPE:

Utility

Patent Application - First Publication

FILE SEGMENT: CHEMICAL APPLICATION OTHER SOURCE: CA 142:5560

NUMBER OF CLAIMS:

80 7 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1A show results of a study demonstrating the effect of temperature on Adp53 production (vp/flask).

FIG. 1B shows results of a study demonstrating the effect of temperature on Admda7 production (vp/flask).

FIG. 2. Cell growth and viability in the bioreactor.

FIG. 3. Glucose and lactate concentrations (g/L) in media vs. days in culture.

FIG. 4. Diagram of a perfusion bioreactor system.

FIG. 5. Cell growth and viability in perfusion culture vs. days in culture.

FIG. 6. Glucose and lactate concentrations (g/L) in perfusion culture vs. days in culture.

The present invention addresses the need to improve the yield of AB adenovirus when grown in cell culture systems. In particular, it has been demonstrated that for adenovirus, the use of infection temperatures lower than 37 degrees C. in a cell culture system results in improved yields of adenovirus. In addition, it has been demonstrated that when host cells are grow in a bioreactor, initiating adenovirus infection by diluting the host cells with fresh media and adenovirus results in improved yield of adenovirus. Methods of adenoviral production and purification using infection temperatures less than 37 degrees C. are disclosed. Methods of adenoviral production and purification wherein the host cells are grown in a bioreactor and adenovirus infection is initiated by diluting the host cells with fresh media and adenovirus are also disclosed.

1.6 ANSWER 7 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN

10654604 IFIPAT; IFIUDB; IFICDB AN

METHODS OF PURIFYING HUMAN ACID TITLE:

ALPHA-GLUCOSIDASE

van der Ploeg; Ans T., Poortugaal, NL INVENTOR(S):

Reuser; Arnold J., Rotterdam, NL

PATENT ASSIGNEE(S): Unassigned

Gary M. Nath; NATH & ASSOCIATES PLLC, 6th Floor, 1030 AGENT:

15th Street, N. W., Washington, DC, 20005, US

NUMBER PK DATE \_\_\_\_\_\_ US 2004161837 A1 20040819 PATENT INFORMATION: US 6118045 A1 ORIGINAL PATENT APPLICATION INFORMATION: US 2004-777644 20040213

US 1996-700760 19960729

ORIGINAL APPLICATION

GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

CONTINUATION-IN-PART OF: US 2001-770253 20010129 ABANDONED

CONTINUATION-IN-PART OF: US 2002-46180 20020116 PENDING

DIVISION OF: US 2001-886477 20010622 ABANDONED

NUMBER DATE

19950802 (Provisional) 20040819 US 1995-1796P US 2004161837 PRIORITY APPLN. INFO.:

FAMILY INFORMATION:

US 6118045

Utility DOCUMENT TYPE:

Patent Application - First Publication

FILE SEGMENT: CHEMICAL

APPLICATION

OTHER SOURCE: CA 141:186901

## PARENT CASE DATA:

The present application is a continuation-in-part of U.S. patent application Ser. No. 09/770,253 filed Jan. 29, 2001 which is a continuation-in-part of U.S. patent application Ser. No. 60/001, 796 filed Aug. 2, 1995, which is now U.S. Pat. No. 6,118,045, granted Sep. 12, 2000 examined as U.S. patent application Ser. No. 08/700,760 filed Jul. 29, 1996 the subject matter of each incorporated by reference herein in their entirety and a continuation-in-part of U.S. patent application Ser. No. 60/111, 291 filed Dec. 7, 1998, which is now published as WO/00/34451 on Jun. 15, 2000 from PCT application US99/29042, filed Dec. 6, 1999 the subject matter of each incorporated by reference herein in their entirety.

NUMBER OF CLAIMS: 39 18 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1: A transgene containing acid  $\alpha$ -glucosidase cDNA. The  $\alpha s1$ -casein exons are represented by open boxes; . alpha.-glucosidase cDNA is represented by a shaded box. The . alpha.s1-casein intron and flanking sequences are represented by a thick line. A thin line represents the IgG acceptor site. The transcription initiation site is marked (), the translation initiation site (ATG), the stopcodon (TAG) and the polyadenylation site (pA). FIG. 2 (panels A, B, C): Three transgenes containing acid  $\alpha$  -glucosidase genomic DNA. Dark shaded areas are  $\alpha s1$  casein sequences, open boxes represent acids  $\alpha s1$  cucosidase exons, and the thin line between the open boxes represents  $\alpha$ -glucosidase introns. Other symbols are the same as in FIG. 1.

- FIG. 3 (panels A, B, C): Construction of genomic transgenes. The  $\alpha\text{-glucosidase}$  exons are represented by open boxes; the .
- alpha.-glucosidase introns and nontranslated sequences are indicated by thin lines. The pKUN vector sequences are represented by thick lines.
- FIG. 4 (panels A and B). Detection of acid  $\alpha$ -glucosidase in milk of transgenic mice by Western blotting.
- FIG. 5. Chromatography profile of rabbit whey on a Q Sepharose FF column.
- FIG. 6. Chromatography profile of Q Sepharose FF-purified \*\*\*recombinant\*\*\* human a-glucosidase fraction on a Phenyl HP Sepharose column.
- FIG. 7. Chromatography profile of a (Phenyl HP Sepharosepurified) \*\*\*recombinant\*\*\* human a-glucosidase fraction on Source Phenyl 15 column.
- FIG. 8. SDS-PAGE analysis of various fractions during the acid aglucosidase
  \*\*\*purification\*\*\* procedure. Various fractions obtained during a
  \*\*\*recombinant\*\*\* human acid a-glucosidase purification
  from rabbit milk (line 60) were diluted in non-reduced SDS sample buffer. The
  samples were boiled for 5 minutes and loaded on a SDS-PAGE gradient gel (4-12%,
  Novex).
- FIG. 9. HPLC size exclusion profile of purified recombinant \*\*\*human\*\*\* acid aglucosidase precursor.
- FIG. 10. Binding of 1251 human acid a-glucosidase precursor to various metal-chelating and lectin Sepharoses. Purified human acid a-glucosidase precursor from rabbit line 60 was radiolabeled with 1251 as described in Example 5. Binding of the labeled enzyme to the metal-chelating Sepharoses (Fe2+, Fe3+, Cu2+, Zn2+, glycine, and control) and to the lectin Sepharoses (Concanavalin A and lentil) was done as described in Example 1. Two washing procedures were tested: either a wash with PBS, 0.002% Tween-20 buffer, or a wash with PBS, 0.1% Tween-20,0.5 M sodium chloride buffer. The binding percentages relate to the total amount of radiolabel added to the tubes.
- FIG. 11. Chromatographic elution profiles of acid a-glucosidasecontaining fractions on various HIC columns.
- FIG. 12 Chromatography profiles of transgenic and non-transgenic whey fractions on a Hydroxylapatite column. Transgenic (----) and non-transgenic (----) rabbit whey, obtained after skimming (by centrifugation) and casein removal (by TFF), were loaded on a Amberchrome column (4.6x150 mm) containing MacroPrep

ceramic hydroxylapatite type I (40 Ltm beads; BioRad) connected to a FPLC system of Pharmacia. Whey fractions obtained after TFF were diluted 5-fold in buffer A (10 mM NaPi pH 6.8), and 0.2 ml was loaded on the column pre-equilibrated in buffer A. The flow rate was 2 ml/min. After loading, bound protein was eluted with a gradient to 500 mM NaPj pH 6.8 in 10 column volumes. Protein was detected by measuring the absorbance at 280 nm (flow cell is 2 mm). FIG. 13. SDS-PAGE analysis of whey fractions from the hydroxylapatite column. Transgenic and non-transgenic rabbit whey were loaded on the Macro-Prep ceramic hydroxylapatite type) column as described in FIG. 12.

FIGS. 14 to 19 are chromatograms of hydroxylapatite chromatography separations of transgenic whey samples in which the samples were loaded on to the column at sodium phosphate buffer (NaPi) concentrations of 5, 10, 20, 30, 40 or 50 mM respectively. The pH of the buffer was 7.0. The chromatograms show the gradient of sodium phosphate eluting buffer to 400 mM, the AZSO and the pH of the eluate and the fractions collected.

FIGS. 20 to 23 are chromatograms of hydroxylapatite chromatography separations as in FIGS. 14 to 19 above except that the pH of the sample was varied whilst the NaPi buffer concentration was retained at 5 mM. The pH of the samples fractionated were pH 6.0, 7.0 and 7.5 respectively.

FIG. 24 is a chromatogram of an industrial (pilot) scale separation of transgenic milk whey on Q Sepharose FF.

FIG. 25 is a chromatogram of hydroxylapatite column chromatography of 0.1 M eluate from the Q Sepharose FF column.

FIG. 26 is a silver stained SDS-PAGE gel of flow through fractions from a series of hydroxylapatite chromatography separations of 0.1 M eluates of Q Sepharose FF.

The invention provides methods of purifying lysosomal proteins, AB pharmaceutical compositions for use in enzyme replacement therapy, and methods of treating Pompe's disease using purified human acid alpha glucosidase.

ANSWER 8 OF 16 CAPLUS COPYRIGHT 2006 ACS on STN DUPLICATE 1

ACCESSION NUMBER:

2003:408803 CAPLUS

DOCUMENT NUMBER:

139:5755

TITLE:

Large scale production and purification of

human recombinant  $\alpha$ -L-

iduronidase for treating mucopolysaccharidosis

INVENTOR(S):

Qin, Minmin; Chan, Wai-pan; Chen, Lin; Fitzpatrick,

Paul A.; Hendstrand, John M.; Wendt, Dan J.; Zecherle,

Gary N.; Starr, Christopher M.; Kakkis, Emil D.

PATENT ASSIGNEE(S):

Biomarin Pharmaceutical Inc., USA

SOURCE:

U.S., 34 pp., Cont.-in-part of U.S. Ser. No. 439,923.

CODEN: USXXAM

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND DATE	APPLICATION NO.	DATE
US 6569661	B1 20030527	US 2000-711202	20001109
US 6426208	B1 20020730	US 1999-439923	19991112
WO 2002038775	A2 20020516	WO 2001-US47843	20011109
WO 2002038775	A3 20040226		
W: AE, AG, AL,	AM, AT, AU, AZ,	BA, BB, BG, BR, BY, BZ,	CA, CH, CN,
CO, CR, CU,	CZ, DE, DK, DM,	DZ, EC, EE, ES, FI, GB,	GD, GE, GH,
GM, HR, HU,	ID, IL, IN, IS,	JP, KE, KG, KP, KR, KZ,	LC, LK, LR,
LS, LT, LU,	LV, MA, MD, MG,	MK, MN, MW, MX, MZ, NO,	NZ, PL, PT,
RO, RU, SD,	SE, SG, SI, SK,	SL, TJ, TM, TR, TT, TZ,	UA, UG, US,
UZ, VN, YU,	ZA, ZW		
RW: GH, GM, KE,	LS, MW, MZ, SD,	SL, SZ, TZ, UG, ZW, AM,	AZ, BY, KG,
KZ, MD, RU,	TJ, TM, AT, BE,	CH, CY, DE, DK, ES, FI,	FR, GB, GR,

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IE, IT, LU, MC, NL, PT, SE, TR, BF, BJ, CF, CG, CI, CM, GA, GN,
             GO, GW, ML, MR, NE, SN, TD, TG
                                            AU 2002-27369
                                20020521
                                                                    20011109
     AU 2002027369
                         A5
                                             US 2001-993038
                                 20021010
                                                                    20011113
     US 2002146802
                          A1
                         Α
                                             ZA 2002-3619
                                                                    20020507
     ZA 2002003619
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                        A1
B2
A1
                                          US 2002-206443
     US 2003013179
                                20030116
                                                                    20020725
     US 704140,
US 2006040348 A1
     US 7041487
                                20060509
                                             US 2003-722371
                                20060223
                                                                    20031124
                                                              20031124
20040823
A2 19991112
A3 20001109
                                20050224
                                            JP 2004-242343
PRIORITY APPLN. INFO.:
                                             US 1999-439923
                                             JP 2002-509470
                                             US 2000-711202
                                                                A 20001109
                                             WO 2001-US47843
                                                                W 20011109
                                             US 2001-993038
                                                                A1 20011113
     The present invention provides a method to mass produce human
AB
     {\tt recombinant} {\tt lpha-L-} iduronidase in large scale amts.
     with appropriate purity to enable large scale production for long term patient
     use of the enzyme therapy. The method comprises the steps of: (a)
     harvesting and filtering fluid obtained from a culture of Chinese hamster
     ovary cells transformed with nucleic acids encoding the human
     recombinant α-L- iduronidase; (b) adjusting the pH
     of the fluid to an acidic pH wherein any potential virus is inactivated
     and said human recombinant a-L-
     iduronidase is not harmed, followed by filtration through a 0.2
     \mu to 0.54 \mu filter; (c) passing the fluid from step (b) through a
     Cibacron Blue dye interaction chromatog. column to capture the
     human recombinant \alpha-L- iduronidase; (d)
     passing the fluid through a copper chelation chromatog. column to remove
     contaminating Chinese hamster ovary proteins; (e) passing the fluid
     through a Ph hydrophobic interaction chromatog. column to reduce residual
     leached Cibacron Blue dye and copper ions canned over from previous
     columns; and (f) concentrating and diafiltering the purified
     human recombinant \alpha-L- iduronidase;
     wherein said purity of equal to or greater than .apprx.99%
     purity of human recombinant α-L-
     iduronidase is measured by µg of contaminating Chinese hamster
     ovary protein per mg of total protein. The purified com. grade
     recombinant human \alpha-L- iduronidase can be
     used for treating genetic disorders including \alpha-L-
     iduronidase deficiency and mucopolysaccharidosis I.
                               THERE ARE 43 CITED REFERENCES AVAILABLE FOR THIS
REFERENCE COUNT:
                         43
                                RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT
L6
     ANSWER 9 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN
AN
                          10268777 IFIPAT; IFIUDB; IFICDB
                          RECOMBINANT ALPHA-L-IDURONIDASE,
TITLE:
                          METHODS FOR PRODUCING AND PURIFYING THE
                          SAME AND METHODS FOR TREATING DISEASES CAUSED BY
                          DEFICIENCIES THEREOF; ENZYMATIC POLYPEPTIDE FOR USE
                          IN THE TREATMENT OF LYSOSOMAL STORAGE DISORDERS
INVENTOR(S):
                          Kakkis; Emil D., Novato, CA, US
                          Tanamachi; Becky, Signal Hill, CA, US
PATENT ASSIGNEE(S):
                          Unassigned
PATENT ASSIGNEE PROBABLE: Los Angeles Biomedical Res Inst at Harbor Ucla
                          Medical Center (Probable)
AGENT:
                          HOWREY SIMON ARNOLD & WHITE, LLP, BOX 34, 301
                          RAVENSWOOD AVE., MENLO PARK, CA, 94025, US
                             NUMBER
                                            PK DATE
                          -----
                                                 -----
PATENT INFORMATION: US 2003013179 A1 20030116 APPLICATION INFORMATION: US 2002-206443 20020725
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GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

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US 1999-439923 CONTINUATION OF: 19991112 6426208

FAMILY INFORMATION: US 2003013179 20030116

US 6426208

DOCUMENT TYPE: Utility

Patent Application - First Publication

FILE SEGMENT: CHEMI CAL

APPLICATION

NUMBER OF CLAIMS: 20 8 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA encoding alpha-L-iduronidase (SEQ ID Nos: 1 and 2). Nucleotides 1 through 6200 are provided. Amino acids are provided starting with the first methionine in the open reading frame.

FIG. 2 represents the results from an SDS-PAGE run of eluate obtained according to the procedure set forth in Example 1. Lane 1 is blank. Lane 2 contained high molecular weight standards. Lane 3 is a blank. Lane 4 contained bovine serum albumin in a concentration of 50 mu g. Lanes 5 through 10 represent eluate containing recombinantly produced human alphaL-iduronidase

in amounts of 1 mu g, 2 mu g, 5 mu g, 5 mu g, 5 mu g and 5 mu g, respectively. FIG. 3 reveals the urinary GAG levels in 16 MPS I patients in relation to normal excretion values. There is a wide range of urine GAG values in untreated MPS I patients. A greater than 50% reduction in excretion of undegraded GAGs following therapy with recombinant alpha-L-iduronidase is a

valid means to measure an individual's response to therapy.

FIG. 4 demonstrates leukocyte iduronidase activity before and after enzyme therapy in MPS I patients.

FIG. 5 demonstrates the buccal iduronidase activity before and after enzyme therapy.

FIG. 6 demonstrates in three patients that a substantial shrinkage of liver and spleen together with significant clinical improvement in joint and soft tissue storage was associated with a greater than 65% reduction in undegraded GAG after only 8 weeks of treatment with recombinant enzyme.

FIG. 7 demonstrates that there is substantial normalization of livers and spleens in patients treated with recombinant enzyme after only 12 weeks of therapy.

FIG. 8 demonstrates a precipitous drop in urinary GAG excretion over 22 weeks of therapy with recombinant enzyme in 6 patients.

AB The present invention provides a recombinant alpha -Liduronidase and biologically active fragments and mutants thereof, methods to produce and purify this enzyme as well as methods to treat certain genetic disorders including- alpha -Liduronidase deficiency and mucopolysaccharidosis I (MPS 1).

L6 ANSWER 10 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN

AN 03902072 IFIPAT; IFIUDB; IFICDB TITLE: RECOMBINANT ALPHA-L-IDURONIDASE,

METHODS FOR PRODUCING AND PURIFYING THE

SAME AND METHODS FOR TREATING DISEASE CAUSED BY

DEFICIENCIES THEREOF

INVENTOR(S): Kakkis; Emil D., Novato, CA

PATENT ASSIGNEE(S): Harbor-UCLA Research and Education Institute,

Torrance, CA, US

PRIMARY EXAMINER:

Achutamurthy, Ponnathapu

ASSISTANT EXAMINER:

Rao, Manjunath N Chiang Robin C. Halluin Albert P.

AGENT:

Howrey Simon Arnold & White LLP

NUMBER PK DATE

US 6585971 B1 20030701 PATENT INFORMATION: APPLICATION INFORMATION: US 2000-711205 20001109

12 Nov 2019 EXPIRATION DATE:

GRANTED PATENT NO.

APPLN. NUMBER DATE OR STATUS

CONTINUATION-IN-PART OF: US 1999-439923 19991112 6426208

FAMILY INFORMATION: US 6585971 20030701

US 6426208

DOCUMENT TYPE: Utility

REASSIGNED

Granted Patent - Utility, no Pre-Grant Publication

FILE SEGMENT: CHEMICAL

GRANTED

OTHER SOURCE: CA 139:73769

PARENT CASE DATA:

This application is a continuation-in-part of U.S. patent application Ser. No. 09/439,923, filed on Nov. 12, 1999 now U.S. Pat. No. 6,426,208, Jul. 30, 2002.

Subject to any Disclaimer, the term of this patent is NOTE:

extended or adjusted under 35 USC 154(b) by 232 days.

011804 FRAME NO: 0640 013922 013989 0436

NUMBER OF CLAIMS: 30

MICROFILM REEL NO:

14 Drawing Sheet(s), 19 Figure(s). GRAPHICS INFORMATION:

DESCRIPTION OF FIGURES:

FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA encoding alpha-L-iduronidase (SEQ ID NOS:1 and 2). Nucleotides 1 through 6200 are provided. Amino acids are provided starting with the first

methionine in the open reading frame. FIG. 2 represents the results from SDS-PAGE runs of eluate obtained according to the procedures as described below. The top panel shows the SDS-PAGE results purified alpha-Liduronidase (3 micrograms) and contaminants from the production/ purification scheme disclosed in Kakkis, et al.,

Protein Expr. Purif. 5: 225-232 (1994). In the bottom panel, SDS-PAGE

results of purified alpha-L-iduronidase with contaminants

from an unpublished prior production/purification process (U.S. patent application Ser. Nos. 09/078,209 and 09/170,977) referred to as the

Carson method in Lanes 2 (7.5 microgram alpha-Liduronidase) and Lane 3 (5.0 microgram alpha-L-iduronidase) are compared to that of the

production/purification process of the present invention referred to as the Galli Process (Lane 4 5 micrograms alpha-L-iduronidase). Lane

1 contains the molecular weight marker. FIG. 2 shows that the Galli production/

\*\*\*purification\*\*\* method of the present invention yields a highly

\*\*\*purified\*\*\* alpha-L-iduronidase product with fewer contaminants

in comparison with prior production/purification schemes.

FIGS. 3A-3B demonstrates the alpha-iduronidase production level over a 30-day period, during which time cells are switched at day 5 from a serum-containing medium to a serum-free medium. alpha-Iduronidase

production was characterized by: (1) absence of a need for adaptation when cells are switched from serumcontaining to serum-free medium at 100200 (top and bottom panels) with an uninterrupted increase in productivity (top panel); (2) a high level of production in excess of 4 mg per liter (1000 per mL) in a

protein-free medium (bottom panel); and (3) a boost in alpha-

\*\*\*iduronidase\*\*\* production with butyrate induction events (bottom panel). FIG. 4 demonstrates a decrease in liver volume during enzyme therapy in MPS I patients.

FIG. 5 demonstrates urinary GAG excretion during enzyme therapy.

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FIG. 6 demonstrates elbow and knee extension in HAC002 during enzyme therapy.
FIG. 7 demonstrates shoulder flexion to 104 weeks in four patients with the
most restriction during enzyme therapy.
FIG. 8 demonstrates improvement in sleep apnea before and after six weeks of
therapy.
FIG. 9 demonstrates the improvement in apneas and hypopneas during sleep with
enzyme therapy in each individual patient.
FIG. 10 demonstrates the improvement in pulmonary function tests before and
after 12 and 52 weeks of enzyme therapy in one patient.
FIG. 11 demonstrates increased height growth velocity with enzyme therapy.
FIG. 12 shows the degree of contamination by Chinese Hamster Ovary Protein
(CHOP) and degree of purity of alpha-Liduronidase, produced by (1) the Carson
method, an unpublished prior production/purification process (U.S.
patent application Ser. Nos. 09/078,209 and 09/170,977 and (2) the Galli
method, the production/purification process of the present invention.
Thus, FIG. 12 shows that alpha-L-iduronidase produced and
***purified*** by the Galli method has a higher degree of purity and lower
degree of CHOP contamination in comparison to that of the Carson method.
     The present invention provides a recombinant human
     alpha -Liduronidase and biologically active fragments and mutants
     thereof, large scale methods to produce and purify commercial
     grade recombinant human alpha -L-iduronidase
      enzyme as well as methods to treat certain genetic disorders including
     alpha -Liduronidase deficiency and mucopolysaccharidosis I (MPS 1).
    ANSWER 11 OF 16 CAPLUS COPYRIGHT 2006 ACS on STN DUPLICATE 2
ACCESSION NUMBER:
                        2002:368665 CAPLUS
DOCUMENT NUMBER:
                        136:385047
TITLE:
                        Methods for large scale production and
                        purification of human \alpha-L-
                        iduronidase for treatment of
                        mucopolysaccharidosis I
                        Qin, Minmin; Chan, Wai-Pan; Chen, Lin; Fitzpatrick,
INVENTOR(S):
                        Paul A.; Henstrand, John M.; Wendt, Dan J.; Zecherle,
                        Gary N.; Starr, Christopher M.; Kakkis, Emil D.
PATENT ASSIGNEE(S):
                        Biomarin Pharmaceutical, Inc., USA
SOURCE:
                        PCT Int. Appl., 71 pp.
                        CODEN: PIXXD2
DOCUMENT TYPE:
                        Patent
LANGUAGE:
                        English
FAMILY ACC. NUM. COUNT:
PATENT INFORMATION:
    PATENT NO.
                      KIND DATE
                                         APPLICATION NO. DATE
                                          _____
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                        A2
                               20020516
                                          WO 2001-US47843
                                                                20011109
    WO 2002038775
                        A3
                               20040226
    WO 2002038775
        W: AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN,
            CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH,
            GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR,
            LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT,
            RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US,
            UZ, VN, YU, ZA, ZW
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RW: GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW, AM, AZ, BY, KG,
             KZ, MD, RU, TJ, TM, AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR,
             IE, IT, LU, MC, NL, PT, SE, TR, BF, BJ, CF, CG, CI, CM, GA, GN,
             GQ, GW, ML, MR, NE, SN, TD, TG
                                             US 2000-711202
     US 6569661
                                20030527
                          B1
                                                                    20001109
     AU 2002027369
                                             AU 2002-27369
                          A5
                                20020521
                                                                    20011109
                                                               A 20001109
A2 19991112
PRIORITY APPLN. INFO.:
                                             US 2000-711202
                                             US 1999-439923
                                             WO 2001-US47843
                                                                W 20011109
AB
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 $\alpha\text{-L-}$  iduronidase and biol. active fragments and muteins thereof with a purity greater than 99%. The present invention further provides large-scale methods to produce and purify com. grade recombinant human a-L- iduronidase enzyme thereof. The method involves preparation of a seed culture containing Chinese hamster ovary cells 2.131 transfected with a vector encoding cDNA for  $\alpha$ -L- iduronidase. These cells is washed and resuspended in a protein-free culture medium supplemented with 7.6 mg/L thymidine, 13.6 mg/L hypoxanthine, 375  $\mu$ g/mL G418 and 5% fetal bovine serum. The cell suspension is incubated at 37°C for 2-3 days with 5% CO2 in three 225 cm flasks. The said cell suspension is split by sequentially adding the cells to one 1L spinner flask, two 3L flasks and 4 8L flasks. The cell suspension is stirred at 50 rpm, followed by increasing the inoculum volume by incubating and subculturing cells to a final cell d. of about 2-2.5 x 105. A mixture containing macroporous microcarriers is prepared in growth medium with fetal bovine serum and transfering said mixture to a bioreactor. Cells from the bioreactor may be harvested at a d. of about 106. Methods for purifn. of α-L- iduronidase to greater than 99% purity include adjusting the pH to an acidic range, followed by filtering the mixture through a 0.2-0.54  $\mu$  filter. The filtrate is further passed through a blue sepharose FF column to capture the protein which purifies a-L- iduronidase 7-10-fold. Contaminating CHO proteins are removed by passing the fluid through a copper chelating sepharose column. The mixture is then passed through a Ph sepharose column to reduce residual leached Cibacron blue dye and copper ions carried over from the previous columns. Purified  $\alpha\text{-L-}$ iduronidase is concentrated and diafiltered. The purifn. steps include 10% glycerol in all buffers to improve the  $\alpha$ -Liduronidase yield. The specific activity of  $\alpha$ -Liduronidase may be greater than 240,000 units/mg protein.

L6 ANSWER 12 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN

AN10221051 IFIPAT; IFIUDB; IFICDB

TITLE: METHODS FOR TREATING DISEASES CAUSED BY DEFICIENCIES

OF RECOMBINANT ALPHA-L-IDURONIDASE

; ENZYMATIC POLYPEPTIDE FOR USE IN THE DIAGNOSIS AND

TREATMENT OF ALLERGIES, HEART AND RESPIRATORY

DISORDERS

INVENTOR(S):

Kakkis; Emil D., Novato, CA, US

PATENT ASSIGNEE(S):

Unassigned

PATENT ASSIGNEE PROBABLE: Los Angeles Biomedical Res Inst at Harbor Ucla

Medical Center (Probable)

AGENT:

HOWREY SIMON ARNOLD & WHITE, LLP, BOX 34, 301 RAVENSWOOD AVE., MENLO PARK, CA, 94025, US

		NUMBER	PK	DATE
PATENT INFORMATION:	US	2002164758	A1	20021107
APPLICATION INFORMATION: 1	US	2001-993241		20011113

	APPLN. NUMBER	DATE	GRANTED PATENT NO. OR STATUS
CONTINUATION OF:	US 2000-711205	20001109	PENDING
CONTINUATION-IN-PART OF:	US 1999-439923	19991112	PENDING
FAMILY INFORMATION:	US 2002164758	20021107	

DOCUMENT TYPE:

Utility

Patent Application - First Publication

20050222

FILE SEGMENT:

CHEMICAL APPLICATION

US 6858206

DESCRIPTION OF FIGURES:
FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA encoding alpha-L-iduronidase (SEQ ID NOS:1 and 2). Nucleotides 1 through 6200 are provided. Amino acids are provided starting with the first methionine in the open reading frame.
FIG. 2 represents the results from SDS-PAGE runs of eluate obtained according to the procedures as described below. The top panel shows the SDS-PAGE results of purified alpha-Liduronidase (3 micrograms) and contaminants from the production/ purification scheme disclosed in Kakkis, et al., Protein Expr. Purif. 5: 225-232 (1994). In the bottom panel, SDS-PAGE

results of purified alpha-L-iduronidase with contaminants from an unpublished prior production/purification process (U.S.

patent application Ser. Nos. 09/078,209 and 09/170,977) referred to as the Carson method in Lanes 2 (7.5 microgram alpha-Liduronidase) and Lane 3 (5.0 microgram alpha-Liduronidase) are compared to that of the

microgram alpha-L-iduronidase) are compared to that of the production/purification process of the present invention referred to as the Galli Process (Lane 4 5 micrograms alpha-L-iduronidase). Lane 1 contains the molecular weight marker. FIG. 2 shows that the Galli production/

\*\*\*purification\*\*\* method of the present invention yields a highly \*\*\*purified\*\*\* alpha-L-iduronidase product with fewer contaminants in comparison with prior production/purification schemes.

FIG. 3 demonstrates the alpha-iduronidase production level over a 30-day period, during which time cells are switched at day 5 from a serum-containing medium to a serum-free medium. alphaIduronidase production was characterized by: (1) absence of a need for adaptation when cells are switched from serumcontaining to serum-free medium at 100200 (top and bottom panels) with an uninterrupted increase in productivity (top panel); (2) a high level of production in excess of 4 mg per liter (1000 per mL) in a protein-free medium (bottom panel); and (3) a boost in alpha-iduronidase production with butyrate induction events (bottom panel).

FIG. 4 demonstrates a decrease in liver volume during enzyme therapy in MPS I patients.

FIG. 5 demonstrates urinary GAG excretion during enzyme therapy.

FIG. 6 demonstrates elbow and knee extension in HAC002 during enzyme therapy.

FIG. 7 demonstrates shoulder flexion to 104 weeks in four patients with the most restriction during enzyme therapy.

FIG.~8 demonstrates improvement in sleep apnea before and after six weeks of therapy.

FIG. 9 demonstrates the improvement in apneas and hypopneas during sleep with enzyme therapy in each individual patient.

FIG. 10 demonstrates the improvement in pulmonary function tests before and after 12 and 52 weeks of enzyme therapy in one patient.

FIG. 11 demonstrates increased height growth velocity with enzyme therapy.

FIG. 12 shows the degree of contamination by Chinese Hamster Ovary Protein (CHOP) and degree of purity of alpha-Liduronidase, produced by (1) the Carson method, an unpublished prior production/purification process (U.S.

patent application Ser. Nos. 09/078,209 and 09/170,977 and (2) the Galli method, the production/purification process of the present invention.

Thus, FIG. 12 shows that alpha-L-iduronidase produced and

\*\*\*purified\*\*\* by the Galli method has a higher degree of purity and lower degree of CHOP contamination in comparison to that of the Carson method.

FIG. 13 shows a comparison of alpha-L-iduronidase produced by the Galli method versus the Carson method. On the left side of the Figure, results from a Western Blot show that the Galli material (left side, column 2) comprise fewer contaminating protein bands (between 48 kDa and 17 kDa) in comparison with the Carson material (left side, column 3). On the right side of the Figure, results from an SDS-PAGE silver stain show the absence of a band at the 62 kDa in the Galli material (column 2) in comparison to the presence of such a band in the Carson material (column 3).

The present invention provides a formulation comprising a pharmaceutical composition comprising a human recombinant alpha -Liduronidase or biologically active or muteins thereof with a

purity of greater than 99%, or in combination with a pharmaceutically acceptable carrier. The present invention further provides methods to treat certain genetic disorders including alpha -Liduronidase deficiency and mucopolysaccharidosis I (MPS 1) by administering said formulation.

L6 ANSWER 13 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN

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METHODS FOR PRODUCING AND PURIFYING TITLE:

RECOMBINANT ALPHA-L-IDURONIDASE;

ENZYMATIC POLYPEPTIDE FOR USE IN GENETIC ENGINEERING

Chan; Wai-Pan, Castro Valley, CA, US INVENTOR(S): Chen; Lin, San Francisco, CA, US

Fitzpatrick; Paul A., Albany, CA, US Henstrand; John M., Davis, CA, US Kakkis; Emil D., Novato, CA, US Qin; Minmin, Pleasanton, CA, US Starr; Christopher M., Sonoma, CA, US Wendt; Dan J., Walnut Creek, CA, US

Zecherle; Gary N., Novato, CA, US

PATENT ASSIGNEE(S): Unassigned

PATENT ASSIGNEE PROBABLE: Los Angeles Biomedical Res Inst at Harbor Ucla

Medical Center (Probable)

HOWREY SIMON ARNOLD & WHITE, LLP, BOX 34, 301 AGENT:

RAVENSWOOD AVE., MENLO PARK, CA, 94025, US

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DOCUMENT TYPE: Utility

Patent Application - First Publication

FILE SEGMENT: CHEMICAL

**APPLICATION** 

NUMBER OF CLAIMS: 7 13 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1 represents the nucleotide and deduced amino acid sequences of cDNA encoding alpha-L-iduronidase (SEQ ID NOS:1 and 2). Nucleotides 1 through 6200 are provided. Amino acids are provided starting with the first

methionine in the open reading frame. FIG. 2 represents the results from SDS-PAGE runs of eluate obtained according to the procedures as described below. The top panel shows the SDS-PAGE results

purified alpha-Liduronidase (3 micrograms) and contaminants from the production/ purification scheme disclosed in Kakkis, et al.,

Protein Expr. Purif. 5: 225-232 (1994). In the bottom panel, SDS-PAGE results of purified alpha-L-iduronidase with contaminants

from an unpublished prior production/purification process (U.S.

patent application Ser. Nos. 09/078,209 and 09/170,977) referred to as the Carson method in Lanes 2 (7.5 microgram alpha-Liduronidase) and Lane 3 (5.0

microgram alpha-L-iduronidase) are compared to that of the

production/purification process of the present invention referred to as the Galli Process (Lane 4 5 micrograms alpha-L-iduronidase). Lane

1 contains the molecular weight marker. FIG. 2 shows that the Galli production/

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in comparison with prior production/purification schemes.
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FIG. 9 demonstrates the improvement in apneas and hypopneas during sleep with
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FIG. 10 demonstrates the improvement in pulmonary function tests before and
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FIG. 11 demonstrates increased height growth velocity with enzyme therapy.
FIG. 12 shows the degree of contamination by Chinese Hamster Ovary Protein
(CHOP) and degree of purity of alpha-Liduronidase, produced by (1) the Carson
method, an unpublished prior production/purification process (U.S.
patent application Ser. Nos. 09/078,209 and 09/170,977 and (2) the Galli
method, the production/purification process of the present invention.
Thus, FIG. 12 shows that alpha-L-iduronidase produced and
                by the Galli method has a higher degree of purity and lower
***purified***
degree of CHOP contamination in comparison to that of the Carson method.
FIG. 13 shows a comparison of alpha-L-iduronidase produced by the
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Figure, results from an SDS-PAGE silver stain show the absence of a band at the
62 kDa in the Galli material (column 2) in comparison to the presence of such
a band in the Carson material (column 3).
     The present invention provides a recombinant human
AB
     alpha -Liduronidase and biologically active fragments and muteins thereof
     with a purity greater than 99%. The present invention further
     provides large-scale methods to produce and purify commercial
     grade recombinant human alpha -L-iduronidase
     enzyme thereof.
    ANSWER 14 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN
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                          10129817 IFIPAT; IFIUDB; IFICDB
AN
                          METHODS OF PURIFYING HUMAN ACID
TITLE:
                          ALPHA-GLUCOSIDASE; PURIFYING PREFERENTIAL
                          ENZYMATIC POLPEPTIDE; OBTAIN SAMPLE, EXPOSE TO
                          COLUMN, RECOVER ELUATE, APPLY TO COLUMN, RECOVER
                          ENZYMATIC POLYPEPTIDE
INVENTOR(S):
                          Reuser; Arnold J., Rotterdam, NL
                          Van der Ploeg; Ans T., Poortugaal, NL
PATENT ASSIGNEE(S):
                          Unassigned
```

NATH & ASSOCIATES, 1030 15th STREET, 6TH FLOOR,

WASHINGTON, DC, 20005, US

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APPLICATION

OTHER SOURCE: CA 137:17456

NUMBER OF CLAIMS: 39 24 Figure(s).

DESCRIPTION OF FIGURES:

FIG. 1: A transgene containing acid  $\alpha$ -glucosidase cDNA. The as1-casein exons are represented by open boxes; . alpha.-glucosidase cDNA is represented by a shaded box. The . alpha.s1-casein intron and flanking sequences are represented by a thick line. A thin line represents the IgG acceptor site. The transcription initiation site is marked (), the translation initiation site (ATG), the stopcodon (TAG) and the polyadenylation site (pA). FIG. 2 (panels A, B, C): Three transgenes containing acid alpha.glucosidase genomic DNA. Dark shaded areas are asl casein sequences, open boxes represent acids alpha.-glucosidase exons, and the thin line between the open boxes represents aglucosidase introns. Other symbols are the same as in FIG. 1.

FIG. 3 (panels A, B, C): Construction of genomic transgenes. The  $\alpha$ -glucosidase exons are represented by open boxes; the .

alpha.-qlucosidase introns and nontranslated sequences are indicated by thin lines. The pKUN vector sequences are represented by thick lines.

FIG. 4 (panels A and B). Detection of acid  $\alpha$ -glucosidase in milk of transgenic mice by Western blotting.

FIG. 5. Chromatography profile of rabbit whey on a Q Sepharose FF column. A whey fraction from rabbit (line 60) milk (about 550 ml), prepared by tangential flow filtration (TFF) of the (diluted) skimmed milk, was incubated with solvent/detergent (1% Tween-80,0.3% TnBP), and loaded on a Q Sepharose FF column (Pharmacia XK-50 column, 18 cm bed height; 250 5 cm/hr flow rate). The column was washed with (7) column volumes (cv) of buffer A (20 mM sodium phosphate buffer pH 7.0), and the human acid a-glucosidase fraction was eluted with 3.5 cv buffer A, containing 100 mM sodium chloride. All strongly bound proteins were eluted with about 3 cv 100% buffer B (1 M NaCl, 20 mM sodium phosphate buffer pH 7.0). All column chromatography was controlled by the AKTA system of Pharmacia.

Protein was detected on-line by measuring the absorbance at 280 nm.

FIG. 6. Chromatography profile of Q Sepharose FF-purified \*\*\*recombinant\*\*\* human a-glucosidase fraction on a Phenyl HP

Sepharose column.

One volume of 1 M ammonium sulphate was added to the Q Sepharose FF acid a-glucosidase eluate (obtained with 100 mM sodium chloride, 20 mM sodium phosphate buffer pH 7.0 step; fraction F3 of FIG. 1) while stirring continuously. This sample was loaded on a Phenyl HP Sepharose column (Pharmacia XK-50 column, 14 cm bed height; 150 cm/hr flow rate) at room temperature (loaded 1-1.2 mg a-glucosidase/ml Sepharose). Before loading, the column was equilibrated in 0.5 M ammonium sulphate, 50 mM sodium phosphate buffer pH 6.0 (=buffer C). After loading the sample, the column was washed with 2 cv of buffer C to remove contaminating proteins like transferrin and serum albumin. Most recombinant human acid a-glucosidase was eluted from the Phenyl HP column with 4 cv buffer D(=50 mM sodium phosphate at pH 6.0 buffer). The strongest bound proteins were eluted first with water, then

with 20% ethanol. FIG. 7. Chromatography profile of a (Phenyl HP Sepharosepurified) \*\*\*recombinant\*\*\* human a-glucosidase fraction on Source Phenyl 15 column. A 2 M ammonium-sulphate, 50 mM sodium phosphate buffer, pH 7.0 was added to the human acid aglucosidase eluate from the Phenyl HP column (fraction F4 from FIG. 6), until a final concentration of 0.85 M ammonium sulphate was reached. The solution was stirred continuously and mildly. The eluate was loaded on a Source Phenyl 15 column (Pharmacia Fineline 100 column, 15 cm bed height ;76 cm/hr flow rate) pre-equilibrated in 0.85 M ammonium sulphate, 50 mM sodium phosphate pH 7.0 buffer (=buffer E). About 2 mg of acid a-glucosidase can be loaded per ml Source 15 Phenyl in this column. After loading the sample, recombinant human acid aglucosidase was eluted from the (Source 15 Phenyl) column with 10 cv of a linear gradient from 100% buffer E to 100% buffer F (buffer F =50 mM sodium phosphate buffer, pH 7.0). Careful pooling of the elution fraction is required (based on purity profiles of the column fractions on SDS-PAGE using Coomassie Brillant Blue staining) to obtain highly purified recombinant acid a-glucosidase. Residual bound proteins were eluted from the column, first with water, and then with 20% ethanol. FIG. 8. SDS-PAGE analysis of various fractions during the acid aglucosidase \*\*\*purification\*\*\* procedure. Various fractions obtained during a \*\*\*recombinant\*\*\* human acid a-gylucosidase purification from rabbit milk (line 60) were diluted in non-reduced SDS sample buffer. The samples were boiled for 5 minutes and loaded on a SDS-PAGE gradient gel (4-12%, Novex). Proteins were stained with Coomassie Brillant Blue. Lane 1: Full rabbit milk (40 ug); 2. Whey after TFF of skimmed milk (40, ug); 3. Acid a-glucosidase eluate fraction from the Q Sepharose FF column (30 ug); 4. Acid aglucosidase eluate fraction from the Phenyl HP column (5 ug); 5. Acid aglucosidase eluate fraction from the Source 15 Phenyl column (5 ug). The letters refer to protein bands which were identified as: a. rabbit immunoglobulins; b. unknown protein; recombinant human acid aglucosidase precursor (doublet under these SDS-PAGE conditions); d. rabbit transferrin, e. rabbit serum albumin; f. rabbit caseins; g. rabbit Whey Acidic Protein (WAP), possibly a dimer; h. rabbit Whey Acidic Protein (WAP), monomer; i. unknown protein, possibly a rabbit WAP variant, or a-lactalbumin; j. dimer or human acid a-glucosidase precursor (doublet under \*\*\*recombinant\*\*\* these SDS-PAGE conditions); k. unknown protein (rabbit transferrin, or processed recombinant human acid aglucosidase. FIG. 9. HPLC size exclusion profile of purified recombinant \*\*\*human\*\*\* acid aglucosidase precursor. Recombinant human acid aglucosidase precursor was purified from transgenic rabbit milk by defatting milk, TFF of skimmed milk, Q FF chromatography, Phenyl HP chromatography. Source 15 Phenyl chromatography, and final filtration. The sample was prepared for the HP SEC chromatography run as described in Example 5. FIG. 10. Binding of 1251 human acid a-glucosidase precursor to various metal-chelating and lectin Sepharoses. Purified human described in Example 5. Binding of the labeled enzyme to the metal-chelating Sepharoses (Fe2+, Fe3+, Cu2+, Zn2+, glycine, and control) and to the lectin

acid a-glucosidase precursor from rabbit line 60 was radiolabeled with 1251 as Sepharoses (Concanavalin A and lentil) was done as described in Example 1. Two washing procedures were tested: either a wash with PBS, 0. 002% Tween-20 buffer, or a wash with PBS, 0.1% Tween-20,0.5 M sodium chloride buffer. The binding percentages relate to the total amount of radiolabel added to the tubes.

FIG. 11. Chromatographic elution profiles of acid a-glucosidasecontaining fractions on various HIC columns.

Purified acid a-glucosidase 110 kDa precursor or mature 76 kDa acid a-glucosidase (A and B; both 5 ug; recombinant from transgenic mouse milk line 2585) were analyzed on a 1 ml Butyl 4 Fast Flow Sepharose or Octyl 4 Fast Flow Sepharose HiTrap column (Pharmacia, Sweden). A transgenic (line 60;-0-) and nontransgenic (-) whey fraction (prepared by 20,000 g, 60 min

centrifugation) were also analyzed on a butyl column (both 200 ul, 25 fold diluted; C). Also a Q Fast Flow fraction (eluted at 100 ut salt from the column; see FIG. 1) of transgenic (line 60;-0-) and non-transgenic (-) whey were loaded on an ether column (both 200 ul, 25-fold diluted; Toyopearl Ether 650 M (TosoHaas) in a 2.5 ml, 5 cm bed height column; C). The results indicate a strong binding of acid a-glucosidase to the HIC columns (A and B). Most whey proteins do not bind (C). A nearly pure acid a-glucosidase was obtained after loading a Q Fast Flow eluate on an ether column (D), where most of the contaminating proteins like serum albumin and transferrin do not bind (SDS-PAGE gels not shown). The binding buffer in A, B, and C was M ammonium sulphate, 50 mM sodium phosphate pH 7.0. The binding buffer in D was 1.5 M ammonium sulphate, 50 mM sodium phosphate pH 7.0. The flow rate was 1 ml/min. Bound protein was eluted with a linear salt gradient to 50 mM sodium phosphate pH 7.0 in 30 min. All column chromatography was controlled by the AKTA system of Pharmacia. Protein was detected on-line by measuring the absorbance at 280 nm (0.2 cm flow cell). The conductivity was measured on line. mAU=milliAbsorbance units, mS/cm=milli-Siemens/cm.

FIG. 12 Chromatography profiles of transgenic and non-transgenic whey fractions on a Hydroxylapatite column. Transgenic (-) and non-transgenic (-) rabbit whey, obtained after skimming (by centrifugation) and casein removal (by TFF), were loaded on a Amberchrome column (4.6 x 150 mm) containing Macro-Prep ceramic hydroxylapatite type I (40 Ltm beads; BioRad) connected to a FPLC system of Pharmacia. Whey fractions obtained after TFF were diluted 5-fold in buffer A (10 mM NaPi pH 6.8), and 0.2 ml was loaded on the column pre-equilibrated in buffer A. The flow rate was 2 ml/min. After loading, bound protein was eluted with a gradient to 500 mM NaPj pH 6.8 in 10 column volumes. Protein was detected by measuring the absorbance at 280 rn (flow cell is 2 mm). FIG. 13. SDS-PAGE analysis of whey fractions from the hydroxylapatite column.

FIG. 13. SDS-PAGE analysis of whey fractions from the hydroxylapatite column. Transgenic and non-transgenic rabbit whey were loaded on the Macro-Prep ceramic hydroxylapatite type) column as described in FIG. 12.

Flow through and eluate fractions were obtained, which were analyzed on SDS-PAGE (for details of the gels see FIG. 8). A. silver stained SDS PAGE of transgenic whey run on hydroxylapatite; B. silver stained SDS PAGE of non-transgenic whey. Up to 6 g protein was loaded.

## DESCRIPTION OF FIGURES:

FIGS. 14 to 19 are chromatograms of hydroxylapatite chromatography separations of transgenic whey samples in which the samples were loaded on to the column at sodium phosphate buffer (NaPi) concentrations of 5,10, 20,30,40 or 50 mM respectively. The pH of the buffer was 7.0. The chromatograms show the gradient of sodium phosphate eluting buffer to 400 mM, the AZSO and the pH of the eluate and the fractions collected.

FIGS. 20 to 23 are chromatograms of hydroxylapatite chromatography separations as in FIGS. 14 to 19 above except that the pH of the sample was varied whilst the NaPi buffer concentration was retained at 5 mM. The pH of the samples fractionated were pH 6.0,7.0 and 7.5respectively.

FIG. 24 is a chromatogram of an industrial (pilot) scale separation of transgenic milk whey on Q Sepharose FF.

FIG. 25 is a chromatogram of hydroxylapatite column chromatography of 0.1 M eluate from the Q Sepharose FF column.

FIG. 26 is a silver stained SDS-PAGE gel of flow through fractions from a series of hydroxylapatite chromatography separations of 0.1 M eluates of Q Sepharose FF. !

The invention provides methods of **purifying** lysosomal proteins, pharmaceutical compositions for use in enzyme replacement therapy, and methods of treating Pompe's disease using **purified** human acid alpha glucosidase.

L6 ANSWER 15 OF 16 IFIPAT COPYRIGHT 2006 IFI on STN
AN 03725200 IFIPAT; IFIUDB; IFICDB
TITLE: RECOMBINANT ALPHA-L-IDIRONIDAS

AB

RECOMBINANT ALPHA-L-IDURONIDASE,
METHODS FOR PRODUCING AND PURIFYING THE
SAME AND METHODS FOR TREATING DISEASES CAUSED BY
DEFICIENCIES THEREOF; ISOLATED POLYPEPTIDE

Kakkis; Emil D., Long Beach, CA INVENTOR (S):

Tanamachi; Becky, Signal Hill, CA

Harbor-UCLA Research and Education Institute, PATENT ASSIGNEE(S):

Torrance, CA

PRIMARY EXAMINER:

Achutamurthy, Ponnathapu

ASSISTANT EXAMINER: AGENT:

Chiang, Robin C. Howrey Simon Arnold & White, LLP

Halluin, Albert P.

Rao, Manjunath N

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NUMBER OF CLAIMS:

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AB The present invention provides a recombinant alpha

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methods to produce and purify this enzyme as well as methods to

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